



Optimization and Modelling for the Remediation of Brilliant Green Dye and Ni²⁺ ions from Water Using Advanced gC₃N₄/PVA@ Alginate Bio-Polymeric Hydrogel Beads

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Abstract

This work offers an innovative technique for creating a ternary composite adsorbent material using ultrasonic synthesis that consists of exfoliated graphitic carbon nitride nanosheets, polyvinyl alcohol, and alginate beads. FTIR, FE-SEM-Mapping, XPS analysis, and X-ray diffraction were among the characterizations that verified the ternary composite beads's successful synthesis and structure. Nickel ion removal and brilliant green (BG) dye adsorption from an aqueous solution were examined using the ternary composite beads' adsorption capabilities, and the influence of pH and the adsorbate's dose was assessed and optimized with response surface methodology (RSM). According to the data, the sorption phenomena are dependent on both the starting concentration of Ni²⁺ & BG dye and pH, with a maximal sorption capacity of 56.8 and 52.2 mg/g for BG dye and Ni²⁺ ions, respectively, at 318K. The Langmuir sorption model provides a good description of the chemisorption process that eliminates Ni²⁺ ions & BG dye, which follows pseudo-second-order kinetics. Additionally, a tenable mechanism for the adsorption of Ni²⁺ ions & BG dye onto the surface of gC₃N₄/PVA@ alginate ternary composite beads is proposed. More importantly, without exhibiting any discernible decrease in sorption ability, gC₃N₄/PVA@ alginate beads frequently used at least five cycles and showed remarkable regeneration ability. The characteristics of the ternary beads and their synthesis method offer a cost-effective and feasible wastewater remediation option.

Keywords: gC₃N₄/PVA@ Alginate Beads; Ni²⁺; BG Dye Remediation; (RSM): Response Surface Methodology

Introduction

The purifying of water for use in drinking, irrigation, industrial processes, and recreational activities is a great environmental task. Physical, chemical, and biological techniques are commonly used in water treatment to eliminate pollutants and toxins from untreated water,

resulting in clear, safe, and clean water. Significant environmental issues, such as water contamination, have been brought on by rapid industrialization and ongoing energy consumption [1]. Due to the serious threat posed by the pollution of water, manufacturing and scientific groups are acting [2,3]. Biological, chemical, or physical techniques may be used to treat potentially toxic substances, relying

on the waste's characteristics. Neutralizing, stabilizing, or isolating hazardous materials to enable their safe disposal or reuse is the aim of dangerous waste treatment [4]. For the decontamination of wastewater, several traditional techniques have been used, including coagulation, flocculation, filtration, membrane separation, sedimentation, and reverse osmosis. Although, these techniques have drawbacks. On the other hand, adsorption offers advantages such as operational flexibility, high-quality output, economical initial capital costs and chemical requirements, and the ability to handle pollutants at low levels of therapy [5]. Heavy metal and metalloid-induced damage to the environment is a worldwide public health issue that has caused great concern because these components' levels are regularly found in many environmental media, particularly water [6-9]. Drinking water distribution lines that contain 8–10% Ni by weight. Ni is an important micronutrient that is needed in very small amounts. According to the US EPA when its level rises over 0.015 mg^{-1} , it becomes hazardous and can lead to problems with breathing, and other several diseases [10,11]. The primary raw materials for the manufacture of household goods, vibrant textiles, paints, printing inks, and other products are now coloring agents and dyestuffs. For example, over 107 kg of textile dyes are consumed year worldwide, and around 106 kg of dyes are released into water streams annually, killing over three million people. Stormwater contains a variety of commercial dyes that may be divided into three main categories: non-ionic (disperse and vat dyes), cationic (basic dyes), and anionic (direct, acid, and reactive dyes). However, cationic dyes generally have the greatest detrimental and poisonous impacts on the environment as a whole and the ecosystem that receives the water. Because of their chemical stability, as well as the mutagenic and cancer-causing effects they have on the oceanic biota, releasing such poisonous dyes into the environment has become a global problem [12-14]. Carbon and nitrogen atoms are organized in a special crystal structure to form graphitic carbon nitride ($\text{g-C}_3\text{N}_4$) a two-dimensional material, its large surface area and catalytic activity are attributed to its porous, honeycomb-like structure. These alluring physicochemical properties have made $\text{g-C}_3\text{N}_4$ an interesting material lately. Unfortunately, its modest specific surface area (SSA) contributes to its relatively limited sorption capability as pure nitride. The most often mentioned methods for resolving the aforementioned issues are element doping, composite creation, and heterojunction construction [15-18]. Numerous adsorbents, such as hydrocarbons, polymers, and organic materials, have been studied. Because composite materials have better sorption effectiveness, there is presently an enormous rise in demand for employing them as beads [19,20]. The addition of a biopolymer containing reactive functional groups like (-OH, -COOH), such as sodium alginate SA, and polyvinyl alcohol PVA promotes an aerogel-like texture. Because they are hydrophobic, biocompatible,

biodegradable, and environmentally friendly, PVA and alginate are both intriguing options to be utilized as sorbents in a variety of ways. Compared to alginate beads, the PVA-alginate bead composite has a greater mechanical strength. This bioplastic's ability to biodegrade without producing contaminants makes it a good candidate to be employed as a sorbent [19,21,22]. The objective of this research is to create ternary composite beads and evaluate how well they adsorb nickel metal ions (Ni^{2+}), and brilliant green dye (BG) from aqueous solutions. Batch adsorption tests are then used to assess the effects of various operating parameters, including contact time, and initial contaminant concentration. The first and second-order rate, intraparticle diffusion, and Boyed models are used to characterize the adsorption kinetics and mechanism; in the meantime, Langmuir and Freundlich's isotherms are used to analyze the adsorption mode. To comprehend the process mechanism, the parameters derived from the adsorption investigations are assessed. Extra care is to demonstrate the nanocomposite's likely long-term efficacy, and particular focus is given to considering the regeneration processes over several cycles.

Experimental

Chemicals

Sodium alginate (Na-alginate) and polyvinyl alcohol (PVA) were provided by Sigma Aldrich, calcium chloride, Nitric acid, and urea were purchased from Fluka, Loba Chemie supplied the brilliant green dye (BG), and NiCl_2 (Ni^{2+}), deionized water was used for creating each experimental mixture.

Preparation of $\text{g-C}_3\text{N}_4$ Nanosheets

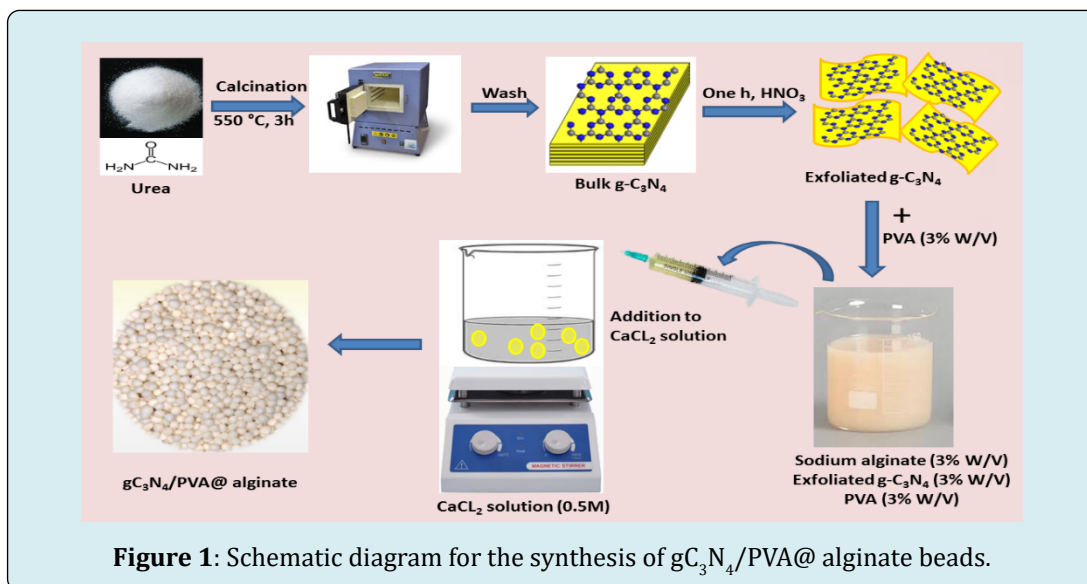
Urea was calcined in a muffle furnace to create the $\text{g-C}_3\text{N}_4$ particles. Usually, a 100 mL ceramic crucible was filled with 20 g of urea then covered, and heated to 550°C for 3 hours at a rate of 2°C per minute. After that, the $\text{g-C}_3\text{N}_4$ was stirringly exfoliated in nitric acid for one hour, then centrifugation was used to gather the exfoliated $\text{g-C}_3\text{N}_4$, which was then left to dry overnight at 65°C [23,24].

Synthesis of $\text{gC}_3\text{N}_4/\text{PVA}@$ Alginate Ternary Adsorbent Beads

Exfoliated $\text{g-C}_3\text{N}_4$ (3% W/V) was dispersed in demineralized water and then sonicated for half an hour, then PVA (3% W/V) and sodium alginate (3% W/V) were introduced, and the resulting amorphous mixture was violently agitated and heated at 50°C for 1 hour till a homogeneous solution is obtained. The combination was injected drop by drop utilizing a syringe pump to an aqueous solution of CaCl_2 (0.5 M) and kept for 6 hours, after which

the beads were completely crosslinked [20,25]. Finally, the obtained $gC_3N_4/PVA@$ alginate beads were washed for 2 hours in distilled water. The pristine alginate beads were

prepared with the same steps without the addition of gC_3N_4 and PVA, the synthesis scheme is presented in Figure 1.



Instrumentation

The IR spectra of synthesized materials have been captured using FT-IR spectroscopy (Shimadzu FTIR-4200) spectrometer. X-ray Diffraction patterns (XRD) of the samples were obtained utilizing a contemporary PAN analytical diffractometer, Xpert PRO type. The prepared catalysts were measured throughout the diffraction angle (2θ) range of 5° and 80° . The surface features of the catalysts were investigated on an HR-SEM (JEOL, JSM model no: 6360). investigation of scanning electron microscopy with energy dispersive X-ray (SEM-EDX) has been accomplished by utilizing scanning electron microscope JEOL GSM 6510LV.

The surface oxidation states and compositional structure were collected via XPS spectra on K-ALPHA (Thermo Fisher Scientific, USA) with monochromatic X-ray Al K- α radiation of -10 – 1350 eV and a spot size of $400 \mu m$ at a pressure of 10 – 9 m bar with a full-spectrum pass energy of 200 eV and a narrow-spectrum of 50 eV. A UV/Vis. spectrophotometer (JENWAY-6505) was utilized for the detection of brilliant green (BG) at λ_{max} of 625 nm. Zetasizer Nano-series HT Malvern instruments were employed to conduct zeta potential analysis. Utilizing atomic absorption spectrophotometry (AAS, ZEE nit 700P/Analytikjena CO., Germany), the liquid's Ni^{2+} contents were assessed.

Batch Adsorption Studies and Parameters Optimization

At a steady temperature of $25^\circ C$ and a stirring speed of 150 rpm, the sorption experiments were conducted in a batch

sequence. To maximize the impact of certain adsorption system variables, including adsorbent dose and pH, on BG dye minimizing efficacy and Ni^{2+} ions onto prepared adsorbents, standard response surface methodology (RSM) based central composite design (CCD) has been employed.

As seen in Table 1, each adsorption parameter has five increased levels: $+\alpha$, $+1$, 0 , -1 , and $-\alpha$. In the models, the pH was adjusted between 3 and 9 , while the dose of adsorbents was adjusted between 0.2 and 1 g/L for both Ni^{2+} ions and BG, respectively. The statistical data analysis was done using the design expert software (V.11).

Factors	Levels				
	$-\alpha$	-1	0	1	$+\alpha$
Adsorbent dose (g/L)	0.2	0.4	0.6	0.8	1
pH	3	4.5	6	7.5	9

Table 1: Experimental factor levels for the removal of BG dye and Ni^{2+} ions by $gC_3N_4/PVA@$ alginate.

The subsequent second-degree polynomial formula characterized the sorption effectiveness trend of the dye and metal ion:

$$Y = \beta_0 + \sum_{i=1}^3 \beta_i X_i + \sum_{i=1}^3 \beta_{ii} X_i^2 + \sum_{i=1}^3 \sum_{j=1}^2 \beta_{ij} X_i X_j \quad (1)$$

Where Y is the response variable, β_0 , β_i , β_{ij} and β_{ii} are the regression coefficients for intercept, linear effect, double interaction, and quadratic effects, respectively, and are

the independent variables.

The removal percentage of BG dyes Ni²⁺ ions was estimated according to Eq. (2):

$$\text{Adsorption (\%)} = \frac{(C_0 - C_e)}{C_0} \times 100 \quad (2)$$

Where, C_0 is the initial concentration and C_e is the concentration at equilibrium.

The capacity (q) of adsorbents was determined at different time intervals and q_t values were calculated by the following equation (3):

$$q_t = \frac{V(C_0 - C_t)}{m} \quad (3)$$

Where q_t (mg/g) is the amount of BG dye or Ni²⁺ ions adsorbed at time t , C_0 (mg/L) is the initial contaminant concentration, C_t (mg/L) is the concentration of a contaminant at time t , V (L) is the volume of the BG dye or Ni²⁺ ions solution, and m (g) is the dry weight of the adsorbent [26].

The adsorption kinetic models of the pseudo-1st-order and pseudo-2nd-order were examined and are presented in linear forms stated as Equations (4 & 5)

$$\log(q_e - q_t) = \log(q_e) - \left(\frac{K_1}{2.303} \right) t \quad (4)$$

$$\frac{t}{q_t} = \frac{1}{(K_2 q_e^2)} + \left(\frac{1}{q_e} \right) t \quad (5)$$

Where, q_t and q_e are the amounts of BG dye or Ni²⁺ ions adsorbed at time t and equilibrium e , respectively; K_1 and K_2 are the pseudo-first-order and pseudo-second-order rate constants, respectively [27].

It is possible to transfer the adsorbent in several stages from the solution phase to the adsorbent surface. The processes could involve pore surface adsorption, film or external diffusion, pore diffusion, and surface diffusion. Adsorption can be finished in one or more steps. The Fickian diffusion laws, which are represented in Eqs. 6 is used to explore intra-particle diffusion.

$$q_t = K_i t^{0.5} + X \quad (6)$$

K_i is the intra-particle diffusion rate (mg/g min^{0.5}), the K_i is the slope of straight-line portions of the plot of q_t versus $t^{0.5}$. X is the intercept, which gives information about the thickness of the boundary layer [28].

Two isothermal sorption scenarios Langmuir and Freundlich were employed to assess adsorption outcomes using the following equations;

$$\frac{1}{q_e} = \frac{1}{K_L C_e Q_m} + \frac{1}{Q_m} \quad (7)$$

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \quad (8)$$

Where, K_L (L/mg) and Q_{max} (mg/g) are the Langmuir constants related to the adsorption energy and sorption capacity, respectively. While, q_e (mg/g) is the equilibrium adsorption capacity and C_e (mg/L) is the equilibrium concentration, also K_f (L/mg) is the Freundlich constant and sorption intensity represented by n which is the heterogeneity factor [27,28].

More information on inherent energetic changes provided by the thermodynamic parameters including Gibbs free energy change (ΔG°), enthalpy change (ΔH°), and entropy change (ΔS°) for the adsorption process which were presented by the following equations;

$$\Delta G^\circ = -RT \ln K_d \quad (9)$$

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ \quad (10)$$

$$\ln K_d = \frac{\Delta S^\circ}{R} - \frac{\Delta H^\circ}{RT} \quad (11)$$

Where R is the ideal gas constant (kJ mol⁻¹ K⁻¹), T is the temperature (K), and K_d is the equilibrium constant [29].

Results and Discussion

Morphology and Structural Characteristics

Studying the sorption behavior of compounds requires an understanding of their surface patterns and elemental composition. As depicted in Figures 2a, 2b the exfoliated g-C₃N₄ consisted of layer-structured 2D discs stacked by uneven nanosheets of varying diameters. In Figure 2c the gC₃N₄/PVA@ alginate micro bead has a rough surface indicating the incorporation of gC₃N₄ nanosheets, while the high magnifications of the bead in Figures 2d, 2e indicates a high porous structure induced by the incorporation of gC₃N₄ and PVA which is highly favorable for the adsorption of dye and metal ion, also the gC₃N₄ nanosheets morphology remains unchanged on the surface of the bead. The high-angle annular dark-field picture (HAADF images in Figure 2f and the elemental mapping analysis that goes along with it displayed in Figures 2g-k indicate the consistent patterns of carbon, nitrogen, oxygen, and calcium in gC₃N₄/PVA@alginate beads. Results displayed in Figure 2l emphasize that the weight percentage of C, N, O, and Ca elements are 45.32, 10.70, 38.83, and 5.15, respectively. Also demonstrates that there were no impurities present when the g-C₃N₄/PVA@BiOCl was prepared.

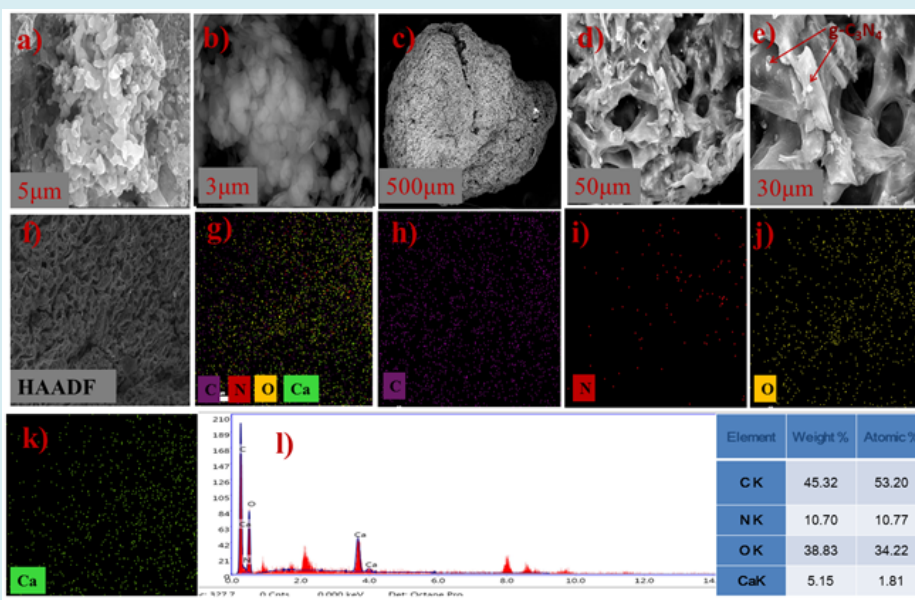


Figure 2: FE-SEM images of (a,b) $g\text{-C}_3\text{N}_4$ at different magnifications, (c) $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ bead, (d, e) high magnifications of $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ bead, (f) HAADF photograph of $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ bead, (g-l) elemental mapping of C, N, O, and Ca, and (l) EDS spectrum of $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ bead.

The crystal structure and phase composition are shown in Figure 3a by analyzing the XRD diffraction patterns of the produced alginate, $g\text{-C}_3\text{N}_4$, PVA, and $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ beads. The amorphous nature of the alginate and PVA polymers was confirmed by the broad peak that displayed at 25° , and 19.49° 2θ respectively [30-32]. The PVA@alginate and $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ beads display a prominent peak at 2θ of 11.97° and 11.87° respectively, which is explained by the alginate, and PVA structure's strong intramolecular and

intermolecular hydrogen bonds. The crystalline patterns of (100) and (002) are correlated with the two main diffraction peaks of $g\text{-C}_3\text{N}_4$ that emerge at 2θ of 13.14° and 27.65° , respectively, the characteristic diffraction patterns pretty well match JCPDS File No. 87-1526 [32,33]. Also, the $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ beads display two peaks at 2θ of 13.81° and 26.87° that correlated to (100) and (002) of $g\text{-C}_3\text{N}_4$ structure. Results indicate the good incorporation of the $g\text{-C}_3\text{N}_4$ and PVA into $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ beads without impurities.

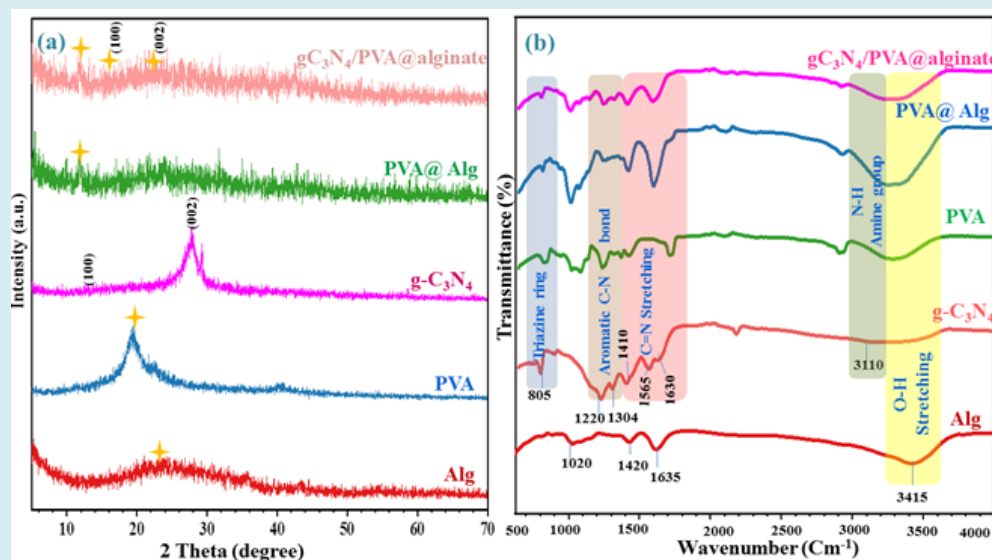


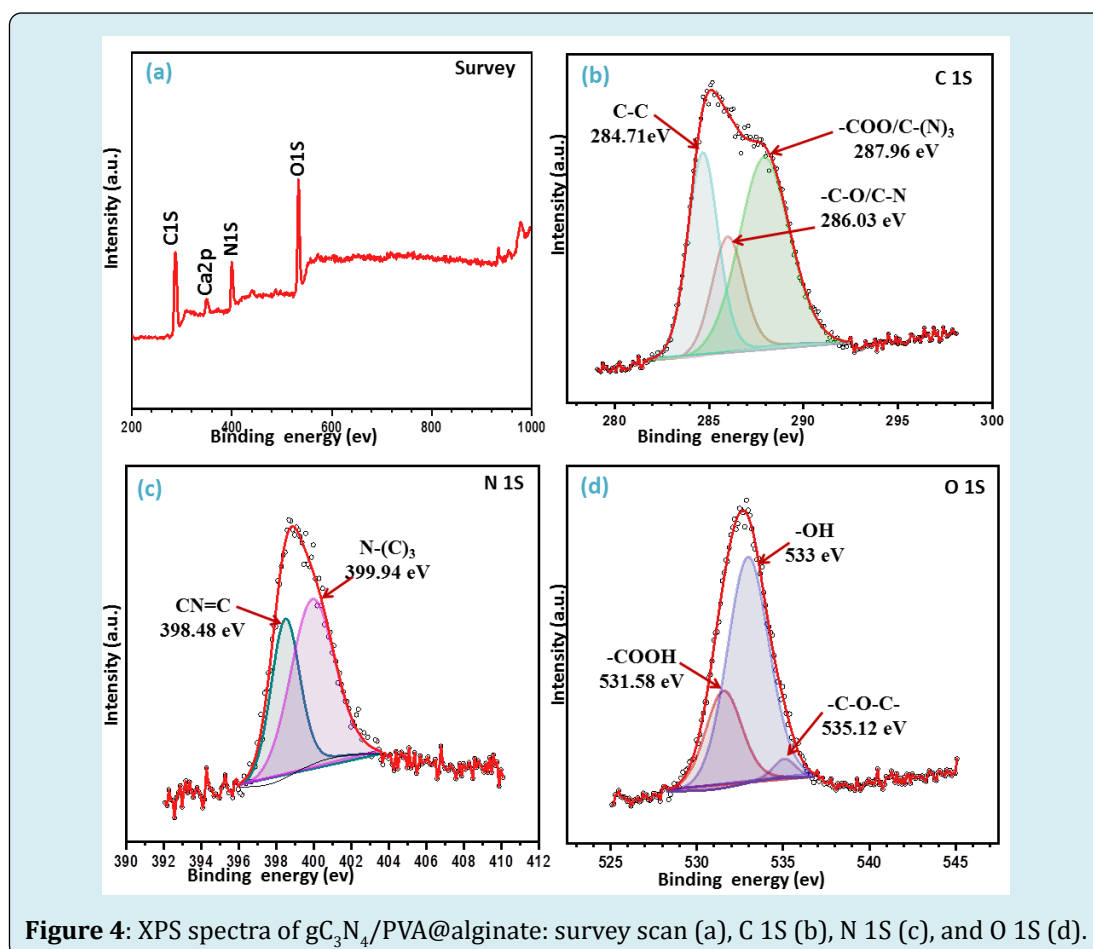
Figure 3: (a) XRD patterns and (b) FT-IR spectra of the alginate, $g\text{-C}_3\text{N}_4$, PVA, PVA@alginate, and $g\text{-C}_3\text{N}_4/\text{PVA@alginate}$ beads.

FT-IR spectroscopy was applied to verify the effective encapsulation of alginate and to Examine the effective groups as illustrated in Figure 3b. Each produced sample displayed a broad peak at 3415 cm^{-1} , which was attributed to the absorbed water molecules' O-H stretching vibrational mode [22,34,35]. The carboxylate groups (O=C-O-) in the alginate polymer are represented by both peaks at 1635 and 1420 cm^{-1} that were seen on the composite microbeads $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ spectra [36,37]. Attributed to the $-\text{NH}_2$ group vibrating, $\text{g-C}_3\text{N}_4$ showed a peak at about 3110 cm^{-1} [38] which shifted to 3090 cm^{-1} in the $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ bead. Similarly, the pattern expanding at 805 cm^{-1} was ascribed to the typical vibration state of the triazine group and appeared in the same position in $\text{gC}_3\text{N}_4/\text{PVA@alginate}$. The bending of aromatic C-N bonds may be one reason for the peaks at 1304 and 1220 cm^{-1} [39-41] that shifted to a higher wavelength at 1319 and 1240 cm^{-1} in the $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ composite. In addition, the peaks that appeared at 1630 cm^{-1} , 1565 cm^{-1} , and 1410 cm^{-1} may be caused by the C=N stretching [42,43] which also shifted to a lower wavelength at 1610 cm^{-1} , 1515 cm^{-1} in the $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads. Generally, all peaks observed in pristine alginate, PVA, and gC_3N_4 are shifted in the composite of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ indicating successful incorporation of gC_3N_4 , PVA into the ternary $\text{gC}_3\text{N}_4/\text{PVA@}$

alginate beads.

The $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads composite's elemental composition and chemical phase were investigated using X-ray photoelectron spectroscopy (XPS).

According to Figure 4a survey spectrum of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$, ternary adsorbent beads consist of the C, Ca, N, and O [44,45] components which improve the absence of impurities. Three peaks at 284.71 eV , 286.03 eV , and 287.96 eV in the high-resolution XPS spectra of C 1s are directed in Figure 4b and can be related to integrated sp^2 C-C bonds, sp^2 -hybridized carbon of C-O and C-N, and sp^3 -coordinated carbon bonds of C-OO and C- N_3 from the $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ surfaces, respectively [31,44]. As shown in Figure 4c, the N 1s peaks at 398.48 eV and 399.94 eV were attributed to sp^2 -bonded N, which belongs to and triazine rings (CN=C) groups and the tertiary nitrogen N-(C) $_3$, respectively [46]. In reference to O1s Figure 4d, three peaks were identified at 5321.58 , 533 , and 535.12 eV , correspondingly attributed to the -COOH, -OH, and C-O-C groups [30]. The effective production of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ ternary beads was verified by XPS.



Evaluation of Adsorption Efficiency in Comparison

At starting Ni^{2+} and BG dye levels of 25 mg/L and sorbent doses of 1 g/L for dried alginate, PVA@alginate, and $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads, a comparison of the adsorption capabilities has been investigated as a function of time. According to Figure 5, BG dye was eliminated by 62.8%, 75.2%, and 95.4% while Ni^{2+} ions were remediated to 61% m

73.8%, and 92% by alginate, PVA@alginate, and $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads, respectively. These results indicate that the incorporation of exfoliated gC_3N_4 and PVA into alginate beads improves its efficiency toward the remediation of dye and heavy metal, which owing to the addition of more function groups and adsorption sites. Thus, all additional adsorption tests using $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads were conducted for different sorption factors.

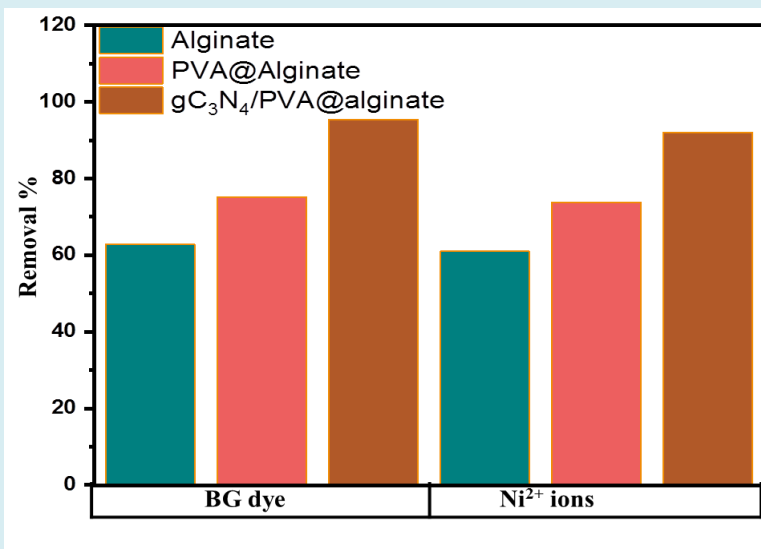


Figure 5: Adsorption efficiencies of alginate, PVA@alginate, and $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads for the removal of BG dye and Ni^{2+} ions.

Response Surface Methodology

Employing central composite design (CCD), researchers can examine how several sorption parameters, like PH and adsorbent dosages, affect brilliant green BG dye and the percentage of Ni^{2+} ions disposed with $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads. CCD is a statistical and computational method that

is useful for data modeling, experimental modeling, and assessing the impact of different factors. The primary benefit of CCD is that it minimizes the number of tests required, explains how the operating variables interact, and optimizes the adsorption circumstances [47]. The results of ANOVA for quadratic model are placed in Table 2.

Adsorbate Source		Std. Dev.	DF	SS	MS	F-value	P-value
BG dye	Model	1.18	5	5609.4	1121.9	41.83	0.0056
	A: PH		1	300	300	11.18	0.0442
	B:Asorbent dose (g/l)		1	2557.9	2557.9	95.36	0.0023
	AB		1	404	404	15.06	0.0303
	A^2		1	933	933	34.78	0.0097
	B^2		1	138	138	5.16	0.1078
	Residual		3	80	27	41.83	0.0056
	Core Total		8	5689.94			

Ni ²⁺	Model	0.21	5	246	49	11.16	0.0373
	A: PH		1	6.7	6.7	1.51	0.3066
	B: Adsorbent dose (g/l)		1	145	145	32.94	0.0105
	AB		1	0.1	0.1	0.0218	0.8921
	A ²		1	41	41	9.28	0.0556
	B ²		1	5.5	5.5	1.24	0.3463
	Residual		3	13	4.4		
	Core Total		8	260	4.4		

Table 2: ANOVA analysis of response surface for removal of toxic heavy metal (Ni²⁺) and brilliant green (BG) by gC₃N₄/PVA@alginate beads.

The degree of freedom (DF), which relates to the overall values employed across the most recent statistical computations that change freely, is a component of an ANOVA investigation. In addition to mean squares (MS), which are linked to an SS split with its appropriate DF and used to compute the F-ratio, the sum of squares (SS) is a computational technique used to evaluate the dispersion of data sets and determine whether data might be matched to a function. A very significant regression model is justified by a lowering P-value (probability) and an increasing F-value, which is a proportion between the model's mean square and residual error. While numbers > 0.05 also have a large impact, the likelihood numbers ≤ 0.05 have a non-significant impact. R² is a regression coefficient that evaluates the correlation between observed and predicted data analytically. Another indicator of fitness is adjusted R², which adjusts the R² values for outcome in the style using the degrees of freedom

computation [48]. In accordance to the adjusted R² outcomes (0.962 & 0.954, respectively), the model R² outcomes show good worth for the removal of BG dye and Ni²⁺ ions by gC₃N₄/PVA@alginate beads (R² = 0.985 and 0.949, respectively). This suggests that the model suggests astonishingly acceptable outcomes to anticipate a response. By measuring the probability value (0.0056 and 0.0373 for both BG dye and Ni²⁺ ions, respectively), which < 0.05 indicated that models have been significant, the model F-values (41.83 and 1.16 for BG dye and Ni²⁺ ions, respectively) demonstrated that statistical analysis has been relevant.

Figure 6 displays the expected results versus actual BG dye and Ni²⁺ removal percentage by gC₃N₄/PVA@alginate beads findings. The results were found to be evenly distributed close to the straight line, indicating an amazing correlation between the anticipated and real output results.

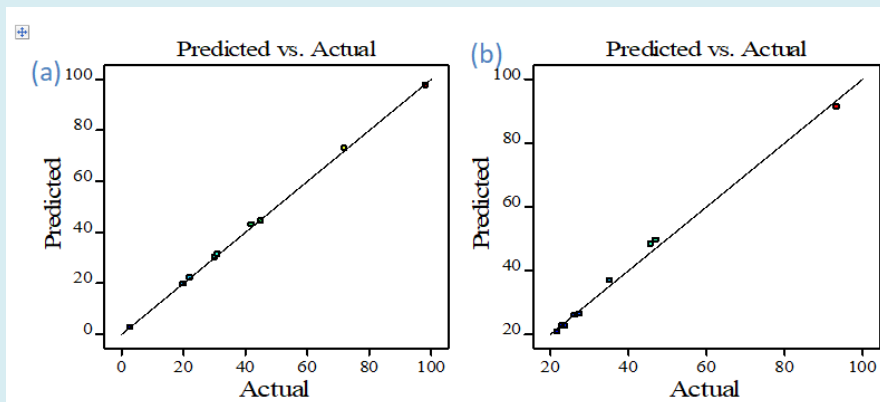


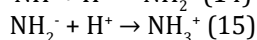
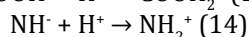
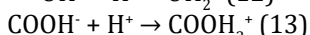
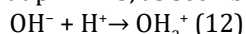
Figure 6: Expected results versus actual results for (a) BG dye and (b) Ni²⁺ removal% by gC₃N₄/PVA@alginate beads.

Combined Influence of Ph with the Adsorbent Doses and Adsorbent Surface Charge

Figures 7(a-d) shows the dual impact of PH and adsorbent dosages on the elimination percentage of BG dye

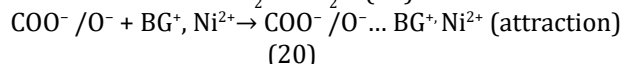
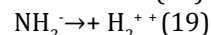
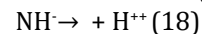
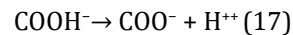
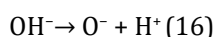
and Ni²⁺ ions 3D surface plots. The effects of PH on BG dye and Ni²⁺ ions sorption ranged from 3-9 at 298 K with initial concentrations of 50 mg/L and reaction time of 4 and 5 hours for BG and Ni²⁺, respectively, because changes in PH have a significant impact on the adsorbent surface-active

groups. Using the adsorbent's surface charge at a specific pH level, the mechanism underlying pH-based dye removal may explain [47]. The remediation of pollutants increased as the pH increased reaching ideal PH values of 7.5 and 6 for BG dye and Ni²⁺ ion, respectively. There are two possible sorption mechanisms (i)chemical reaction among the reactive compounds in BG or Ni²⁺ ions and the -NH, -NH₂, -COOH and -OH groups of gC₃N₄/PVA@alginate beads, which causes these individuals to adsorb on the outermost layer, and (ii) the mechanism of electrostatic interaction between the protonated and deprotonated divides of the adsorbent with the BG dye or Ni²⁺ ions. The gC₃N₄/PVA@alginate beads's surface is protonated at pH < 7.5, as seen below:



$\text{NH}_2^+ / \text{NH}_3^+ / \text{COOH}_2^+ / \text{OH}_2^+ + \text{BG}^+, \text{Ni}^{2+} \rightarrow \text{NH}_2^+ / \text{NH}_3^+ / \text{COOH}_2^+ / \text{OH}_2^+ \dots \text{BG}^+, \text{Ni}^{2+}$ (repulsion)

The BG dye and Ni²⁺ ion adsorption improved progressively at pH values of 7.5 and 6, where deprotonation takes place and free nitrogen and oxygen is released from the gC₃N₄/PVA@alginate bead surface. This increases adsorption by generating electrostatic attraction with the cations.



A higher pH should lead to more BG dye and Ni²⁺ ion adsorption because the adsorbent has more negatively charged surface sites, which creates electrostatic attraction [49-51].

However, more adsorbent surface area and active sites were made available as the dose rose. Also, the findings shown in Figures 7a-d indicate that raising the adsorbent dose from 0.2 to 1 g/L increased the removal percentage to 98.3% and 93.42% for BG and Ni²⁺, respectively. As adsorbent dosage rises, function binding groups are more prevalent on the sorbent surficial layer, which can be explained by a rise in the adsorbent's surface area and active sites [52]. The model demonstrated the optimal conditions for the remediation of BG dye Ni²⁺ ions by gC₃N₄/PVA@alginate beads were an adsorbent dose of 1 g/L with PH of 7.5 and 6 for BG and Ni²⁺ respectively, with actual removal 98.3% and 93.42%, for BG and Ni²⁺, Furthermore, the maximum adsorption capabilities for BG and Ni²⁺ were determined to be 45.3 and 38.71 mg/g, respectively. Based on the ideal conditions that the RSM/CCD developed model produced, additional adsorption experiments were conducted.

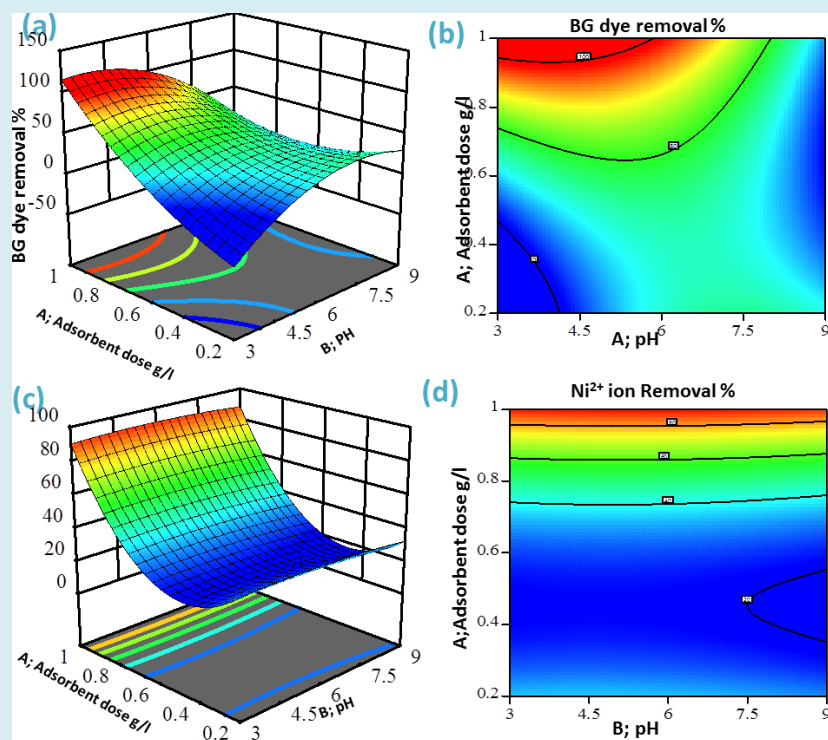


Figure 7: 3D-interaction effect plots of pH and adsorbent doses (a,c), contour plots (b,d) for adsorption of BG dye and Ni²⁺ ion, respectively, using gC₃N₄/PVA@alginate beads.

Effect of Contact Time on the Adsorption Capacity and Kinetics Study

At an initial concentration of 25 ppm and an adsorbent dose of 1g/L for both BG and Ni²⁺, with PH values of 7.5 and 6 for BG and Ni²⁺, respectively, the removal effectiveness of gC₃N₄/PVA@alginate beads concerning contact time was investigated. Figure 8a demonstrates how adsorption on gC₃N₄/PVA@alginate beads increases the elimination of nickel and BG dye over time. Because BG dye and Ni²⁺ ions had a greater possibility of being adsorbed by binding active sites. Because most of the adsorbent sites were saturated, the removal capacities for the adsorption of BG dye and Ni²⁺ ions grew more slowly and progressively from 60 to 90 to 180 minutes, after 180 minutes, no change in removal capacities was seen.

Additionally, Figure 8b displays the UV-visible spectra of brilliant green dye solutions following varying adsorption times with gC₃N₄/PVA@alginate beads; the bands at 625 nm exhibit a decrease in intensity, indicating that they have been removed by adsorption. With removal capabilities of 24.09 and 15.3 mg/g for BG dye and Ni²⁺ ions, respectively, the removal efficiency reached equilibrium at 240 and 300 minutes. Pseudo-1st order, pseudo-2nd order, and fickian diffusion law kinetic models have been examined using the kinetic study results of the adsorption equilibrium time study with the ideal parameters of brilliant green dye and nickel ions sorption behavior evaluated with the response surface methodology. Table 3 discusses the outcomes that were achieved.

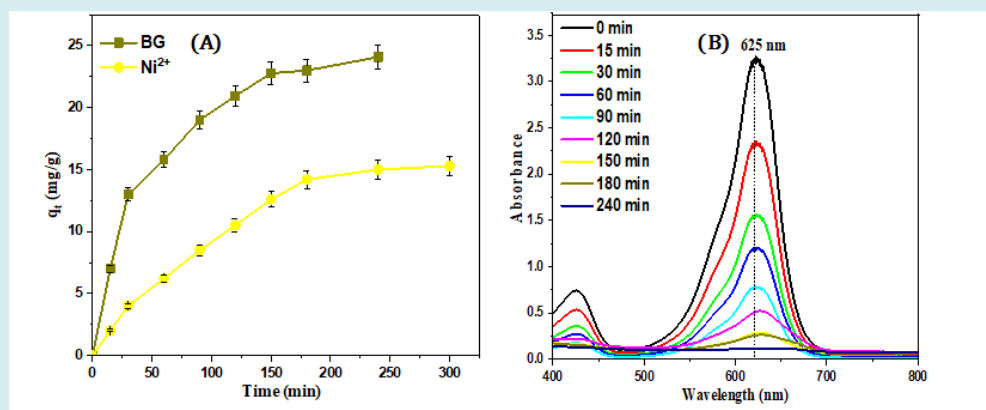


Figure 8: (A) Equilibrium time of brilliant green and nickel ions adsorption onto gC₃N₄/PVA@alginate beads, and (B) UV-Vis absorption spectra of Brilliant green solution in the presence of gC₃N₄/PVA@alginate beads at different times.

Kinetics Model	Kinetics Parameters	BG	Ni ²⁺
Pseudo-first order	R ²	0.93	0.832
	K ₁ (min ⁻¹)	0.0138	0.0023
	q _{e,cal} (mg/g)	42.2	50.53
Pseudo-Second order	R ²	0.997	0.97
	K ₂ (g/mg min)	0.0008	0.00024
	q _{e,cal} (mg/g)	24.2	16.08
Intra particle diffusion	R ²	0.927	0.965
	K ₁ (mg/g min ^{0.5})	1.431	1.079
	X	4.119	1.709

Table 3: Kinetic parameters of pseudo-first order, pseudo – second order and fickian diffusion law kinetic for sorption of Brilliant green BG and Ni²⁺ onto gC₃N₄/PVA@alginate beads (adsorbent dose of 1g/L and PH of 7.5 for BG and 6 for Ni²⁺) with initial concentration of 25 mg/L for both BG and Ni²⁺ at 298 K.

Kinetic designs have been used to analyze data and identify the mechanism underlying the sorption phenomena. Figures 9 A,9B shows the graph of the pseudo-1st order, pseudo-2nd design linearized kinetic equation for both BG and Ni²⁺ gC₃N₄/PVA@alginate beads that are best fitted with pseudo-2nd design, which has high correlation coefficient values R² (0.997 & 0.970). It was suggested that a chemical reaction between sorbent and BG dye, Ni²⁺ occurred during adsorption, involving active sites in the gC₃N₄/PVA@alginate beads surface that incorporated valance forces by sharing or transferring electrons. Low correlation coefficient values for both BG and Ni²⁺ were shown with pseudo-1st order design R² values of 0.930 and 0.832, respectively [53,54].

The R2 values (0.927 and 0.965) of graphing qt against t^{0.5} toward removal of both BG dye and Ni²⁺ ions with gC₃N₄/PVA@alginate, respectively, for the Fickian intra-particle diffusion model shown in Figure 9c suggest that intra-particle diffusion model plays a significant role in degrading BG dye and Ni²⁺ ions, which had intercepts of

4.119 and 1.709, respectively, that \neq zero, indicating that the line does not pass through the origin and highlighting the importance of other adsorption mechanisms in addition to

the rate-controlling step of the intra-particle diffusion model [55].

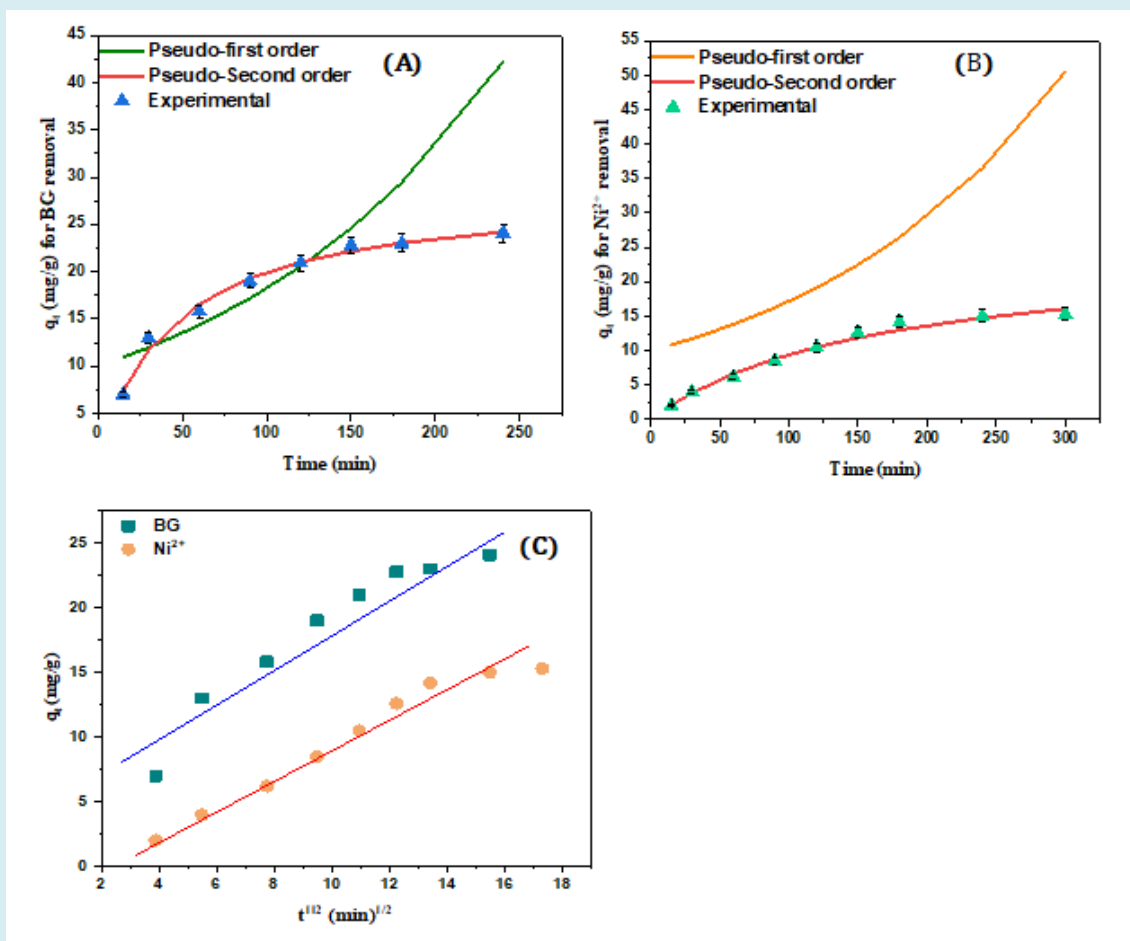


Figure 9: Fitting of (A) BG dye, (B) Ni^{2+} ions adsorption for both pseudo-1st order, pseudo-2nd order adsorption kinetic model, and (C) Fickian intra-particle diffusion model onto $\text{gC}_3\text{N}_4/\text{PVA}@$ alginate beads

Effect of the Initial BG Dye and Ni^{2+} Concentration on the Adsorption Capacity and Isothermal Study

The starting dosage has a direct impact on the rate of adsorption and is an essential variable in adsorption investigations. The direct relationship amongst an adsorbent surface's accessible binding sites and the concentration of either BG dye or Ni^{2+} ions determines the impact of the initial BG dye and Ni^{2+} ions concentration factor [56].

At starting concentrations of 5, 15, 25, 40, 50, and 60 for BG dye and 25, 50, 100, 150, 200, 250, and 300 mg/L for Ni^{2+} ions, pH of 7.5 and 6 for both respectively, and adsorbent dose of 1g/L, at 298 K, Figures 10a,10b illustrates the effect of BG dye and Ni^{2+} ion adsorption by $\text{gC}_3\text{N}_4/\text{PVA}@$ alginate beads. The sorption capacity increased from 4.7 to 46 mg/g

when the concentration of BG dye raised from 5 to 60 mg/L, and from 15.3 to 42 mg/g when the concentration of Ni^{2+} ions raised from 25 to 300 mg/L. This represents a result of the adsorbents' limited quantity of active binding sites. Following a specific level, the adsorbents became saturated and all of these active sites were packed with dye and metal ion molecules. However, the quantity of dye molecules rose as the concentration gradient grew, increasing the pushing force between the liquid and solid phases, which aids in overcoming the dye molecules' resistance to mass transition [57]. Sorption isotherms are crucial for solid-liquid adsorption systems because they provide insight into the adsorption capacity at a given temperature and clarify the interaction between the adsorbent and adsorbate. The dual models that are frequently utilized to explain equilibrium adsorption are the Freundlich and Langmuir isotherm models [58].

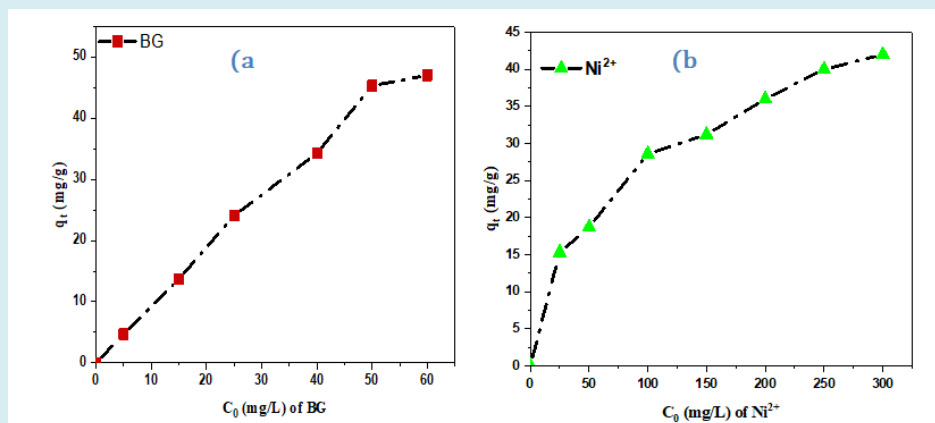


Figure 10: The effect of the initial concentration of (a) BG and (b) Ni^{2+} on adsorption capacity of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads.

The Langmuir and Freundlich isothermal models have been used to assess the obtained data in Figures 10a,b. Table 4 lists the correlation coefficient R^2 values and variables determined for the two equilibrium styles. Additionally, Figures 11a & 11b displays the fitting of the two isothermal equations for the sorption of both BG and Ni^{2+} by $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads.

Adso rbate	Langmuir Model				Freundlich Model		
	Q_L (mg/g)	K_L (L/mg)	R^2	R_L	K_f (mg/g)	n	R^2
BG	47.1	2.76586	0.934	0.598	13.8452	1.73	0.818
Ni^{2+}	44.2	41.5472	0.979	0.802	6.88652	3.09	0.976

Table 4: Isothermal parameters of Langmuir and Freundlich for sorption of B dye and Ni^{2+} ions onto $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads.

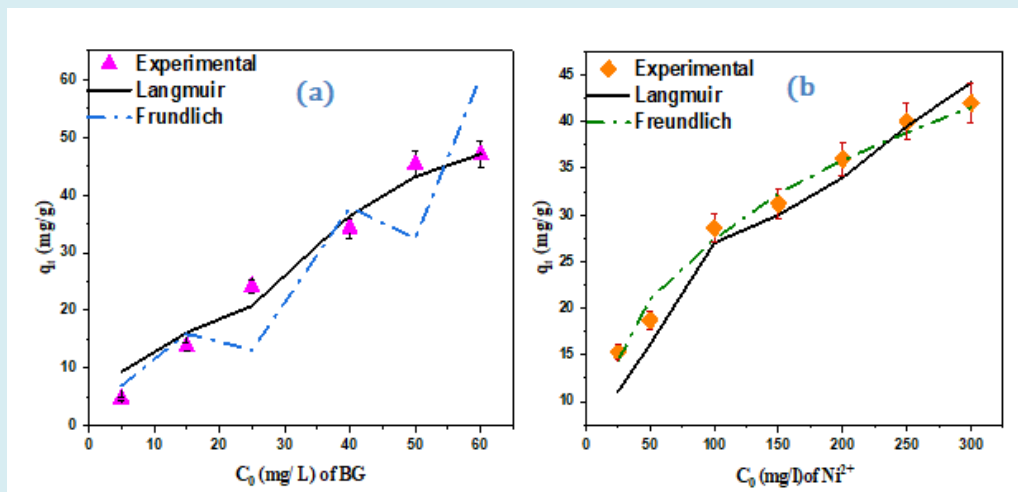


Figure 11: Comparison of the fit of the Langmuir and Freundlich isotherm models for the experimental data of adsorption of (a) BGB and (b) Ni^{2+} onto $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads.

The correlation coefficient amounts suggested a stronger fit for Langmuir than Freundlich styles to describe BG dye sorption into $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads, based on the outcomes shown in Table 4. According to the Langmuir perspective, BG dye is absorbed uniformly by the monolayer on the surface of the bead with equivalent sorption energy and no dye-molecule interaction [59]. On the other hand, the

sorption of Ni^{2+} suggested that the Freundlich and Langmuir models suit $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads well. This implies that the monolayer integrates both homogeneous and heterogeneous Ni^{2+} ion sorption onto the bead's surface with equal sorption energy and without molecule interaction. Furthermore, the heterogeneity styles are improved by good fitting to the Freundlich model, and the Freundlich

parameters are found to confirm that the values of n for BG and Ni^{2+} are 1.73 and 3.09, respectively, suggesting that the sorption is favorable. The K_L value for the sorption of Ni^{2+} ions was greater than that of BG, suggesting that Ni^{2+} binds to the bead surface more strongly than it does to BG dye. The dimensionless constant known as the separation factor (R_L), which used to notify the impacts of Langmuir isotherma [60].

$$R_L = 1 / (1 + K_L C_0) \quad (21)$$

Where C_0 (mg/L) is the starting concentration and K_L (L/mg) is the Langmuir constant related to sorption energy. According to the R_L value, sorption properties are irreversible when $R_L =$ zero, linear when $R_L = 1$, and undesired when R_L is < 1 . Sorption mechanism of BG dye and Ni^{2+} is advantageous for the Langmuir isothermal concept, as indicated by the computed R_L in Table 4, which is 0.598 and 0.802 for both, respectively.

Effect of Temperature on the Adsorption Capacity and Thermodynamic Study

The adsorption temperature, which varied between 298 K and 318 K, at optimal pHs of 7.5 and 6, an adsorbent dosage of 1g/L for BG dye and Ni^{2+} ions, respectively, experiments were done utilizing a 20 mL contaminated solution containing 60, 300 ppm of BG dye and Ni^{2+} for six hours. The temperature has a significant effect on BG dye and Ni^{2+} ions uptake, according to the dynamic data results in Figure 12a at three distinct temperatures. The adsorption mechanism is positively impacted by temperature, as evidenced by the adsorption capacity increasing with temperature, reaching 56.8 and 52.2 mg/g for BG dye and Ni^{2+} ions, respectively, at 318K. The existence of active sites for sorption is increased and the porosity of the adsorbent pore volume is improved by temperature. As the temperature rises, the viscosity of the solution reduces, increasing the rate at which the adsorbate diffuses through the adsorbent's inner and outer pores. This implies that the process of adsorption is endothermic [61]. To find out more about the energy changes and if an adsorption process is spontaneous, thermodynamic analysis can be used to study any sorption phenomena. The Van't Hoff equation was used to compute the thermodynamic parameters, such as Gibb's free energy change (ΔG°), enthalpy change (ΔH°), and entropy change (ΔS°) beads.

Table 5 lists the thermodynamic data obtained by graphing $\ln K_d$ versus $1/T$ in Figure 12b. An endothermic mechanism was proposed by the positive ΔH° amounts for BG dye and Ni^{2+} ions adsorption. Similarly, a significant ΔS° value for the adsorption of BG dye and Ni^{2+} suggests an increase in randomness at the solid-liquid interface throughout the adsorption process. Notwithstanding the large temperature range, BG dye adsorption showed negative ΔG° values,

indicating spontaneous adsorption, but Ni^{2+} adsorption showed positive ΔG° values, indicating nonspontaneous adsorption onto $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads. The fact that ΔG° rose with temperature indicates that the mechanism can tolerate higher temperatures [62] initial dye concentration, adsorbent dose, the particle size of CHAC Z, agitation speed, temperature, and contact time was explored. The equilibrium adsorption data were analyzed using two widely applied isotherms: Langmuir, Freundlich. Best fits were found to be Freundlich isotherm. Langmuir adsorption capacity (Q_m . Enthalpy change values larger than 0.04 kJ/mol are indicative of chemical adsorption but values less than 0.04 kJ/mol are indicative of physical adsorption, per published research. In this investigation, the enthalpy changes for the adsorption of BG dye and Ni^{2+} ions were 66.31 and 10.18 kJ/mol, respectively. Thus, BG dye and Ni^{2+} ions adsorption onto $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads occurs by chemical adsorption.

Pollutant	Temp. (K)	K_d	ΔG°	ΔH°	ΔS°
			(KJ/mol)	(KJ/mol)	(KJ/mol/K)
BG dye	298	3.285714	-2.9473	66.31	0.232
	308	6.692308	-4.8678		
	318	17.75	-7.6047		
Ni^{2+} ions	298	0.162791	4.4975	10.18	0.0192
	308	0.193317	4.2083		
	318	0.210654	4.1179		

Table 5: Thermodynamic parameters for removing BG dye and Ni^{2+} ions onto PPy- $\text{gC}_3\text{N}_4/\text{PVA@alginate}$.

Regeneration and Stability Investigations

From an economic perspective, adsorbents' regeneration and long-term stability are important characteristics. Experiments for reuse & desorption using ethanol solution were conducted to examine the regeneration and stability of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads for the adsorption of BG dye and Ni^{2+} ions. The BG dye and Ni^{2+} ion removal capacities in the first cycle were 46 and 42 mg/g, respectively. The adsorption capacity was assessed for every cycle, and by relating it to the initial run (adsorption capacity being 100%), the relative adsorption capacity was calculated in percentage terms. Figure 13 illustrates the recuperation of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads for five cycles, it was obvious that following the fifth adsorption-desorption goes the efficiency of $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ beads maintained with high absorbing capacity for both BG dye and Ni^{2+} ions 94.3% and 91.25% i.e. 43.37 and 38.32 mg/g, respectively, without significant loss. This demonstrates that the $\text{gC}_3\text{N}_4/\text{PVA@alginate}$ bead's functional groups were not significantly lost and that the composite adsorbent exhibits long-term stability, allowing for post-recycling reuse.

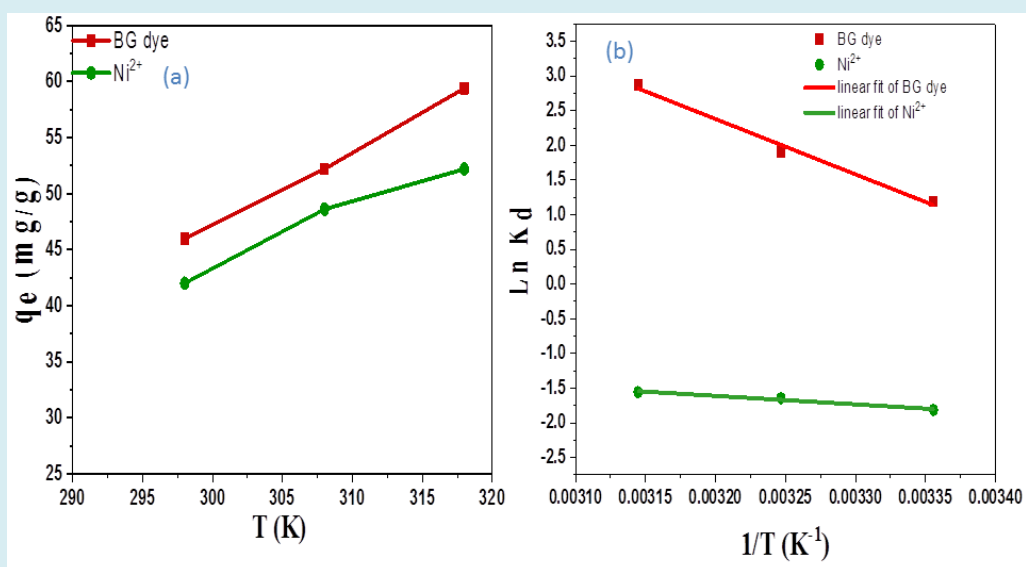


Figure 12: Effect of temperature on the adsorption of BG dye and Ni^{2+} (a), Van't Hoff equation for adsorption of BG dye and Ni^{2+} onto $gC_3N_4/PVA@alginate$ beads (b).

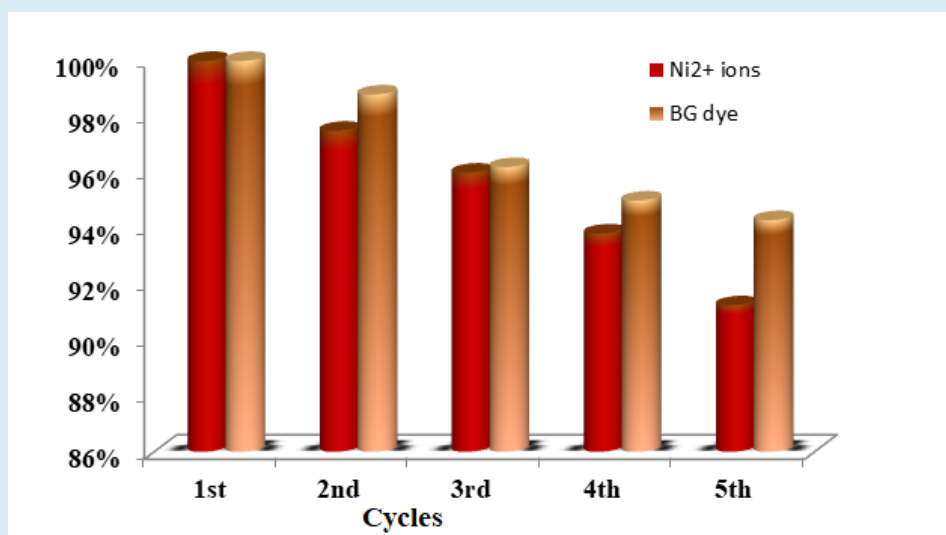


Figure 13: Reuse of $gC_3N_4/PVA@alginate$ bead for the removal of BG dye and Ni^{2+} ions for five cycles

Mechanism of BG dye and Ni^{2+} Elimination from Water

To clarify the potential eradication mechanism for BG dye and Ni^{2+} ions adsorption by $gC_3N_4/PVA@alginate$ beads, FTIR analysis was performed before and after BG dye and Ni^{2+} ions sorption and displayed in Figure 14. A discernible shift in the location of particular peaks in the sorbent was observed upon adsorption. Following the adsorption procedure, the broad peak at 3415 cm^{-1} that corresponded to the O-H group and the band assigned to the carboxylate groups ($O=C-O-$) in the alginate polymer at 1635 and 1420 cm^{-1} were displaced.

Furthermore, there was a shift in the position of the N-H group peak at 1630 cm^{-1} in gC_3N_4 , indicating that additional processes helped to increase the removal of BG dye and Ni^{2+} ions. Electronegative oxygen in $O=C-O$ groups found in alginic beads can connect with heavy metal cations firmly by electrostatic attraction force. However, by complexation, N centers in gC_3N_4 can draw in the heavy metal ions. It is noteworthy that the oxygen centers found in the alginic beads' hydroxyl ($-OH$) and carboxylate ($-COO-$) groups are strong, easily accessible sites that can interact with positively charged BG dye and Ni^{2+} ions through cation exchange and chelation.

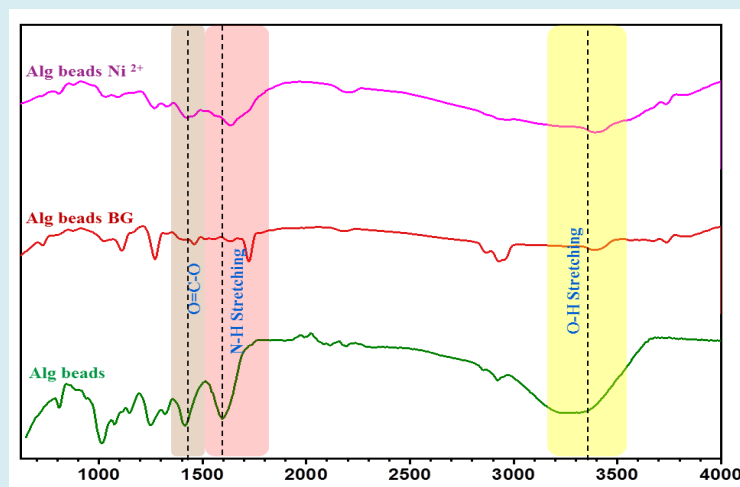


Figure 14: FT-IR spectra of $gC_3N_4/PVA@alginate$ beads before and after BG dye and Ni^{2+} ions adsorption.

Conclusion

In the current study, BG dye and Ni^{2+} ions were remediated from their aqueous solutions by adsorption onto $gC_3N_4/PVA@alginate$ beads. Sorption variables were optimized utilizing Response surface methodology (RSM), indicating optimal remediation performance of 98.3% and 93.42%, for either BG dye and Ni^{2+} , respectively, at pH of 7.7, 6 with sorbent dosages of 1 g/L. Also, either BG dye and Ni^{2+} sorption obeyed pseudo-2nd order concepts, and was a good match for the Langmuir model for BG, while Ni^{2+} sorption was strongly matched for Langmuir and Freundlich isothermal concepts. Furthermore, there was a rise in randomness thus the sorption process was spontaneous with endothermic characteristics.

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